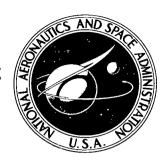
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FLOWMETER FOR SPACE

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FLOWMETER FOR SPACE

SUMMARY

The task of developing a suitable flowmeter to support orbital inspection and checkout operations of large space stations and interplanetary vehicles was undertaken. The objective was approached in a three-phase effort; Phase I, prototype design; Phase II, prototype fabrication and test; Phase III, final design and documentation.

The design phase of this contract resulted in a preliminary prototype design utilizing an orifice-meter measuring system. This system consisted of the following three subsystems: (1) gas handling and conditioning system, (2) orificing system, and (3) pressure measurement system.

After the preliminary design had been developed and approved, a prototype flowmeter was built and tested, first by the contractor and then by Marshall Space Flight Center. The contractor's test program consisted of functional checkout, altitude ascent rate, and flow calibration. MSFC made further tests to (1) verify calibration of flowmeter, (2) calibrate the instrument over the entire meter range, (3) determine the effects of external pressure variations, (4) verify operation with helium, and (5) determine the adequacy of temperature control system.

The technical design and operation of the prototype was so successful that final design was directed primarily toward human engineering factors and safety considerations. A documentation package was developed, including drawings, instructions, and specifications for a flight worthy mass flowmeter. Planning calls for procurement and testing of flight prototype hardware for performance evaluation and environmental qualification pending funding approval.

INTRODUCTION

Current planning for future space exploration indicates the need for a suitable flowmeter to support orbital inspection and checkout operations of large space stations and interplanetary vehicles prior to launch from parking orbits. Most existing flowmeters are either dependent upon earth gravity for

operation or are sensitive to the effects of gravity. Their operation is also designed around the earth environment and is greatly affected by the pressure at the meter outlet.

This program was undertaken to develop a mass flowmeter for measuring flow rates from purges and collected leaks at leak ports, on aerospace hardware, discharging into a space environment. The objective was to be accomplished in a three-phase effort: Phase I, prototype design; Phase II, prototype fabrication and test; and Phase III, final design and documentation.

To ensure that the instrument would be suitable for use by an astronaut in space, several design and operational requirements were placed on the contractor. Most notable of these requirements was the ability to measure the flow of all common gases such as hydrogen, helium, nitrogen, oxygen, and organic vapors, at rates as low as 5 secm and as high as 650 secm in the space environment of zero-gravity with pressures ranging from 1. 333×10^{-1} to 1. 333×10^{-11} N/m² (1 × 10⁻³ to 1 × 10⁻¹³ torr) and with temperature extremes of 70° to 500° K.

DESCRIPTION

Design

The design phase of this project resulted in a preliminary prototype design utilizing an orifice-meter measuring system. The basis of this system is the measurement of the pressure drop across a restriction in the gas stream. Because of the low ambient pressure of outer space, upstream pressure equals ΔP and the restriction can be selected so that it always operates in the supercritical regime. Thus, knowing the gas characteristics, temperature, and pressure, the flowrate is readily determined by

$$Q = 11.4K a^2 P \sqrt{\frac{T}{M}}$$

where a is the orifice radius, K is the flow coefficient, M is the molecular weight of gas, P is the upstream pressure, T is the gas temperature, and Q is the gas flow.

To make these measurements and determine the flowrate, the prototype flowmeter was designed with three main subsystems: (1) the gas handling and conditioning system, (2) the orificing system, and (3) the pressure measurement system.

Gas Handling and Conditioning System. The gas handling and conditioning system was designed to receive the flow from a leak or purge port, conduct it through a temperature conditioning chamber to the orifice manifold, and exhaust it into space. The gas handling portion is rather straightforward, using standard AN fittings and tubing. The temperature conditioning, however, is rather unusual. Normally in flow measurement, a correction is applied to the indicated flow for variations in temperature, but, in this system, the temperature of the gas is maintained within certain limits and the flow is read directly. It is feasible to regulate the gas temperature in this particular application since the maximum flow measurable is a relatively small mass, and heat transfer to the space environment is only by radiation.

The radiation to space was controlled by building the flowmeter case as a box within a box and utilizing "superinsulation" between the walls. This "superinsulation," developed for insulating cryogenic tanks on the Saturn program, consists of multiple layers of aluminized Kapton film and is effective as an insulator only when the ambient pressure is $1.333 \times 10^{-1} \, \text{N/m}^2 \, (10^{-3} \, \text{torr})$ or less. This design limited the heat loss from the package to approximately $1.4 \, \text{watts}$ when exposed to $20 \, \text{°K}$ and the heat gain to $2.9 \, \text{watts}$ when exposed to $500 \, \text{°K}$.

The temperature of the gas entering the orifice manifold is regulated by passing the gas through a chamber attached to a large heat sink. Since the mass of the gas is small and velocity through the chamber is low, the gas stabilizes at the temperature of the heat sink. The sink is heated by resistance elements powered from a rechargeable 9-volt battery and controlled by a 300°K (80°F) thermostat. Cooling is accomplished by a rather unique method, that is, by a canister of dodecahydrate of sodium biphosphate attached to the heat sink. This hydrated salt loses its water of crystallization between the temperatures of 306°K (92°F) and 322°K (120°F), and, in the process of becoming a liquid, it absorbs approximately 14×10^4 joules (39 watt-hours) of energy per 0.4536 kg (1 lb). The process is fully reversible. When hot gas enters the flowmeter, the hydrated salt melts, absorbs heat from the gas, and effectively controls the temperature. Overall, the temperature of gas entering the orifice manifold is maintained between 297°K (75°F) and 325°K (125°F); the heaters do not allow the temperature to drop below 297°K, and the hydrated salt keeps the temperature at 325°K or less.

It might appear that this wide range over which the temperature can fluctuate would introduce a large error in the flow measurement. However, this is not the case. In the mass flow equation, temperature appears as (T) $^{1/2}$, With mass flow varying inversely with the square root of the absolute temperature, a 305° K (90° F) mean temperature with $\pm 30.5^{\circ}$ K ($\pm 55^{\circ}$ F) variation would produce a maximum flow error of only 5 percent. This is an acceptable error in this application; however, it should be noted that this is a worst case and the actual error for a particular reading would normally be much better.

Calculations revealed that heat loss caused by 650 sccm of nitrogen gas entering the instrument at 20°K is 3.8 watts and the heat gain with a gas temperature of 500°K is 2.5 watts. Combining the effects caused by gas temperature and radiation to space, the total worst case heat loss is 5.2 watts and heat gain is 5.4 watts. The battery selected has approximately 7.9×10^4 joules (22 watt-hours) of energy available and the salt canister has approximately 7.2×10^4 joules (20 watt-hours) of energy, giving a minimum operational life of approximately 5 hours at high gas flow at lowest ambient temperature and about 3.1/2 hours at high gas flow at highest ambient temperature.

Orificing System. The orificing system is the heart of the operation of the flowmeter, and the principle of operation is one of basic simplicity. The gas flow to be measured is brought to the previously described temperature range (297° to 325°K) and exhausted to space through an orifice. In this application the exhaust pressure (space vacuum) is very low, ensuring that the flow orifices are always operating in the supercritical regime. Thus the flow through the orifice is dependent only upon the upstream pressure, and, for a given gas, a given orifice, and a given pressure gage, the mass flow can be expressed with good accuracy by:

$$Q = K (\%P) ,$$

where Q is the mass flow, K is the calibration constant, and %P is the pressure gage reading in percentage of full scale.

The wide variety of gases to be measured and the wide range of flow-rates required that more than one orifice be used to obtain accurate readings with a single pressure gage and also hold measurement time within the specified 90 seconds. Calculations using the critical orifice flow equation estab-

lished that three orifices would be adequate. A 0.0439-cm (0.0173-in.) diameter orifice, the smallest, was chosen to measure the minimum hydrogen flow, and the intermediate orifice, with a 0.0782-cm (0.0308-in.) diameter, was chosen to measure the minimum nitrogen flow as well as the high flow of hydrogen. The largest orifice, 0.2667-cm (0.105-in.) diameter, was chosen to measure the upper flow ranges of nitrogen and oxygen and at the same time give adequate capacity for gases of higher molecular weight. The proper orifice for a flow measurement is selected with a toggle valve.

The orifice holes were produced by the "Elox" electromachining process in 0.005-cm (0.002-in.) and 0.0127-cm (0.005-in.) stainless steel. It was found that piercing single plates resulted in burrs, but by sandwiching several plates together the interior plates would be free of burrs. Because of the fragile nature of the orifice plates, they are individually mounted between bezels and can be changed through the bottom of the enclosure by dismounting only the exhaust duct. The orifice plates are also protected by a system relief valve that vents the orifice manifold directly to the space environment.

Pressure Measurement System. The last major subsystem of the flowmeter, the pressure measurement system, performs the actual flow sensing and displays the numerical value. The main item of this system is a pressure gauge with a full scale pressure of 20 inches of water. The particular gauge selected for the prototype is a fairly rugged gauge and can withstand 100 percent overpressure without change of calibration. It has been qualified for ground support equipment use, but further qualification will be necessary prior to use in a flight experiment.

As explained previously, the orifices in this device operate in the super-critical regime, making mass flow through the orifices directly proportional to the upstream pressure. It is a straightforward procedure to calibrate the pressure meter for the various gases. The meter scale can be either marked with percent of full scale and calibration curves used to give actual flowrate, or a multiple scale can be used with flowrate being read directly. Either approach has merit, and the final determination will be made through flight experiment development.

The pressure gauge is protected from destructive overpressure by two devices, a system relief valve and a gauge overpressure cutoff valve. The system relief valve was mentioned earlier in conjunction with protection of the orifice plates. Venting to protect the orifices also relieves pressure to the gauge. The gauge overpressure cutoff valve, in series with the gauge, is diaphram operated and closes when line pressure exceeds a preset value of

 7.47×10^3 N/m² (30 inches of water.) This is a fast-acting device that is used regularly to protect gauges of this type from pressure surges.

A thermometer is also included in the pressure measurement system, but it is physically mounted on the orifice manifold. Here it measures the actual temperature of the gas, allowing the determination of a temperature correction factor for application to the measured flow if the ultimate accuracy of the system is required for a particular measurement. The thermometer also serves another useful purpose in that it indicates proper operation of the temperature control system. If the temperature drops below 297°K (75°F), a malfunction in the electrical circuit is indicated while temperature in excess of 325°K (125°F) indicates the need for recharging the salt canister.

Test

After the preliminary design had been developed and approved, a prototype flowmeter (Fig. 1) was built and tested. Testing was first conducted by the contractor and then the flowmeter was turned over to MSFC for further test, verification, and acceptance.

Contractor Test Program. The contractor test program consisted of (1) functional checkout, (2) altitude ascent rate, and (3) flow calibration.

Functional checkout. The functional checkout was initiated with a leakage check using a helium mass spectrometer. The leakage was determined to be less than 10^{-8} atm cc per second with all selector valves closed.

To test the functioning of the overpressure protection devices, the inlet was over pressured to $16.19 \times 10^3 \ \text{N/m}^2$ (65 inches of water), which is approximately five times the maximum design pressure and 50 times the design flowrate of the flowmeter. The protective devices actuated properly and subsequent tests of the flowmeter showed no indications of damage.

The thermal control heating circuit was operated for approximately one week (from an external power source to conserve the battery) in a bell jar at a pressure of approximately 26.66 N/m² (200 microns). The thermal load was such that the typical thermostat cycle was 30 seconds on and 2 minutes off, resulting in an average power consumption of 1.4 watts. Temperature was maintained within 0.55°K (1°F) with no indication of change of set point.

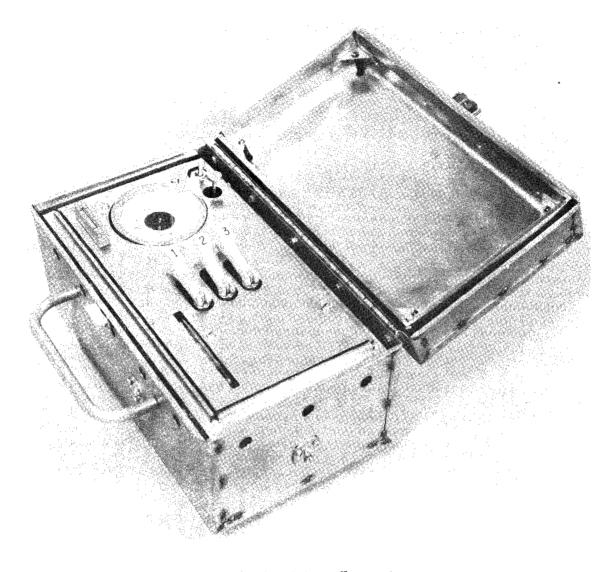


Figure 1. Prototype flowmeter.

Altitude ascent rate. To simulate the reaction of the flowmeter to a take off pressure profile, the prototype flowmeter was placed in a bell jar and rapidly depressurized. The maximum depressurization rate obtainable with the pump used dropped the pressure from atmospheric to $1.333 \times 10^2 \; \text{N/m}^2$ (1 torr) in 32 seconds. This is much more severe than any actual takeoff profile. At this high depressurization rate, the maximum pressure gauge deflection was approximately half scale with only the small orifice being open and the inlet fitting capped off. No disturbances were seen in the multilayer thermal insulation. Also, a test was conducted to determine the effects of

rapid repressurization that would occur when returning from a space vacuum into the spacecraft through an airlock. This test showed that the flowmeter could be repressurized at a maximum rate of 3. 45×10^4 N/m² (5 psi) per second without over pressurizing the gauge element.

Flow calibration. After the various subsystems were determined to be operating properly, the flowmeter was calibrated with nitrogen gas. The flowrate was measured by timing the displacement of a known volume of gas at constant temperature and pressure. The volume of gas was displaced from a calibrated glass cylinder by an oil piston. The flowmeter was placed in a glass bell jar pumped by a mechanical pump rated at 4.25×10^{-1} m³ (15 cfm). This pump was able to maintain the following orifice pressure ratios over a major portion of the flow range of each orifice: orifice number 1, 7.5; orifice number 2, 100; and orifice number 3, 350. In actual use the flowmeter would discharge into space, producing higher orifice pressure ratios. However, the test ratios obtained were well above critical and the calibration error was quite small, more than acceptable for verification of the prototype operation.

MSFC Test Program. Upon completion of testing by the contractor, the prototype flowmeter was delivered to MSFC for further tests and acceptance. The objectives of these tests were as follows:

- 1. To verify the calibration of the flowmeter.
- 2. To calibrate the instrument over the entire meter range using nitrogen.
- 3. To determine the effects of variations of external pressure on the flowmeter.
- 4. To make verification tests using helium.
- 5. To determine the adequacy of the temperature control system.

The flowmeter was tested in a small vacuum chamber pumped by a 50.8-cm (20-in.) diffusion pump and a 14.5 m³ (500 cfm) mechanical pump. A vacuum range of 6.65×10^{-2} N/m² (5×10^{-4} torr) was attainable for full flow through orifice number 2. For orifice number 1, only the large mechanical pump was used and was capable of chamber pressures below 26.6 N/m² (2×10^{-1} torr) for the largest flowrates. Failure of the diffusion pump forced orifice number 3 to be tested using only the mechanical pump. Therefore, the vacuum range for this orifice, about 3.99 N/m² (3×10^{-2} torr), was not as high as desired.

Flowrate was measured by timing the displacement of a predetermined volume of gas at a known temperature and pressure. The displacement was accomplished using a VOL-U-METER.

For each orifice, the nitrogen calibration data were taken first, then pressure variation data were taken for pressures up to $1.333 \times 10^2 \ \text{N/m}^2$ (1 torr), and finally, several data were taken using helium gas. All flow rates were converted to flows at an orifice temperature of 297.6°K (76°F). To make this conversion,

$$\frac{Q_1}{Q_2} = \left(\frac{T_2}{T_1}\right)^{1/2}$$

where Q is the flowrate and T is the absolute temperature of orifice.

The results of the nitrogen flow calibrations are shown in Figures A-1 and A-2 in the Appendix. In all the curves, the abscissa is the observed reading of the pressure gauge. Figure A-1 shows the actual data points (corrected for an orifice temperature of 297.6°K) along with the contractor's calibration curves. The agreement of the two calibration curves was excellent for the two smaller orifices. For the large flow orifice, the data for the two curves deviated, but this discrepancy was caused by the higher capacity vacuum capabilities at MSFC. All data obtained were repeatable and consistent within 2 percent of a linear function.

The data obtained using a helium leak source were also consistently linear and repeatable, behaving in a similar manner to the nitrogen data. A theoretical prediction of the helium data was made from the nitrogen data using the molecular weights and specific heats of the two gases as follows:

$$\frac{Q_{\text{He}}}{Q_{\text{N}_2}} = \left(\begin{array}{c} \frac{M_{\text{N}_2}}{M_{\text{He}}} \end{array} \right)^{1/2} \frac{\left(\frac{k-1}{1+\frac{k-1}{2}} \right)^{\frac{k+1}{k-1}}}{\left(\frac{k}{1+\frac{k-1}{2}} \right)^{\frac{k+1}{k-1}}} \frac{He}{\frac{k+1}{k-1}}$$

where M is the molecular weight, k is the ratio of specific heats, and Q is the mass flow.

Figure A-2 shows the helium data and the theoretical curve obtained from the nitrogen data. The helium data varied about 10 percent from predictions, showing that a calibration for each gas to be measured will probably be necessary.

The flowmeter was tested in a vacuum range of 1. 333×10^2 N/m² (1 torr) to 1. 333×10^{-2} N/m² (1 × 10^{-4} torr) to determine the effects of external pressure. Figure A-3 shows the flow coefficient (at a constant flow-rate) plotted against external pressure. The maximum deviation of the flow coefficient introduced at these extremes was 6 percent. However, most of the deviation occurs above 1. 333×10^{-1} N/m² (1 × 10^{-3} torr), making this problem negligible in a high vacuum environment.

Testing the temperature control system with the flowmeter in the vacuum chamber became an insurmountable problem and had to be abandoned. The mass flowrate and velocity of the gas through the meter was so low that heat transfer between the gas, the interconnecting equipment, and the atmosphere brought the gas to ambient temperature prior to entering the temperature conditioning section of the flowmeter. Gas could not be supplied to the flowmeter with sufficient temperature (high or low) to activate the regulating circuits. A test was made at ambient conditions by bleeding vapor from an LN₂ Dewar directly into the flowmeter. This actuated the heater circuit as the temperature dropped below 297°K (75°F). Although the heater could not handle this unreasonably high cryogenic flow, the regulating circuit operated properly.

Final Design

Since little effort was made in the initial design and test phase to produce a prototype that approached flight configuration, a final design and documentation effort was conducted to develop a complete documentation package for a flyable mass flowmeter. The original technical design and the operation of the prototype proved so successful that this final effort was directed primarily toward human engineering factors and safety considerations. Typical of this effort was the removal of all sharp edges or projections that could be detrimental to the astronaut or his protective clothing, enlargement of the carrying handles to be compatible with the space suit gloves, and modification of the toggle valve lever for visibility and foolproof operation. One minor design deficiency was discovered and corrected. A spirit type thermometer was originally specified to measure gas temperature; however, in the zerogravity of space, these do not function accurately; that is, the fluid separates

and migrates randomly through the capillary tube. A bimetallic type temperature indicator was found to correct this problem. Figure 2 is an artist's sketch of the flowmeter in the final configuration.

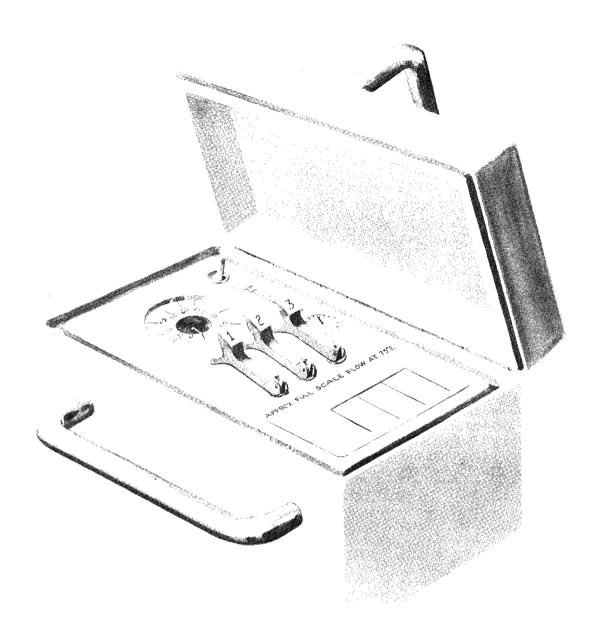


Figure 2. Final configuration of flowmeter.

The documentation package contains complete drawings, instructions, and specifications to allow competitive procurement of the mass flowmeter.

The following table summarizes the operating characteristics of the flowmeter.

Approximate	overall	weight
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Overall package size including handles and inlet fitting $(L \times W \times H)$

Ambient temperature range

(760 torr)]

Maximum operating back pressure to insure thermal insulation

Maximum operating back pressure to insure flow metering accuracy

Approximate full scale flow at 297° K (75° F) [sccm at 293° K (68° F), 10.13×10^4 N/m²

3.51 kilograms (7-3/4 pounds)

0.317 \times 0.235 \times 0.216 meter (12-1/2 \times 9-1/4 \times 8-1/2 inches)

20°K to 500°K

 $1.333 \times 10^{-1} \text{ N/m}^2 \text{ (10}^{-3} \text{ torr)}$

 $1.333 \text{ N/m}^2 (10^{-2} \text{ torr})$

Orifice	1	2	3
Hydrogen	9500	850	270
Helium	7000	650	200
Nitrogen	2500	250	75
Oxygen	2400	225	70

Orifice pressure at full scale flow

 $49.8 \times 10^2 \text{ N/m}^2$ (20 in. H₂O)

Battery specifications:

Type

Storage, Sealed Silver Zinc

 7.9×10^4 joules (22 watt-hours)

Number of cells

6

Voltage of full charge

Approximately 9 volts

Approximate full charge energy recoverable

Heat Sink Specifications:

Туре

Utilizes latent heat of crystallization of NaH PO₄ • 12H₂O, rechargeable

Temperature range of crystallization phase change

306°K to 322°K (92°F to 120°F)

Inlet Connection:

0.635 cm (1/4 inch) female flare (AN)

CONCLUSIONS AND RECOMMENDATIONS

The development of a mass flowmeter designed specifically for use in outer space has proved to be highly successful. A thorough concept study and preliminary design resulted in a prototype flowmeter whose performance was well within contract limitations and exceeded operational requirements. A firm basis exists for building flight hardware for use in space.

The next step to be taken is the procurement and testing of flight prototype hardware for performance evaluation and environmental qualification. Plans are being made to initiate this effort in fiscal year 70. With successful accomplishment of this follow-on, the final effort will be a flight experiment or engineering demonstration.

George C. Marshall Space Flight Center

National Aeronautics and Space Administration

Marshall Space Flight Center, Alabama 35812, August 25, 1969

APPENDIX

NITROGEN FLOW CALIBRATION, HELIUM DATA, AND EFFECT OF PRESSURE VARIATION

The following graphs were not plotted according to SI units, and the conversion would distort their meaning; therefore, the original units have been retained.

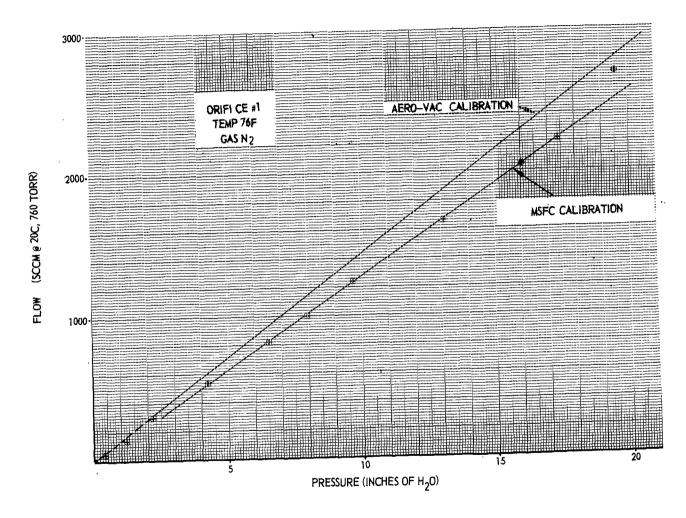


Figure A-1. Nitrogen flow calibration.

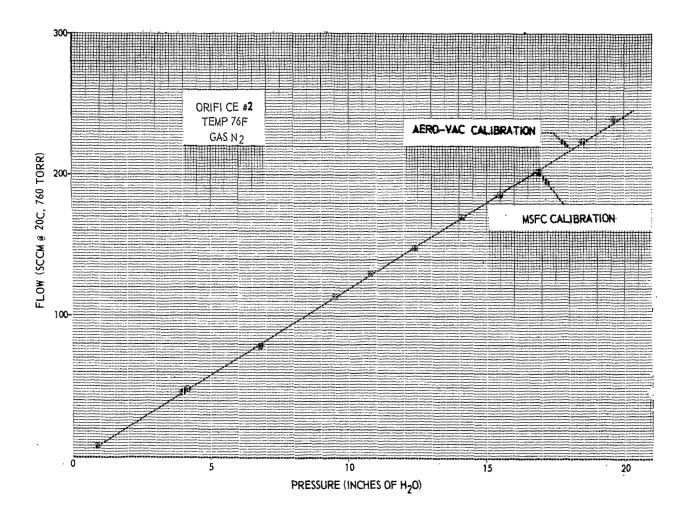


Figure A-1. (Continued).

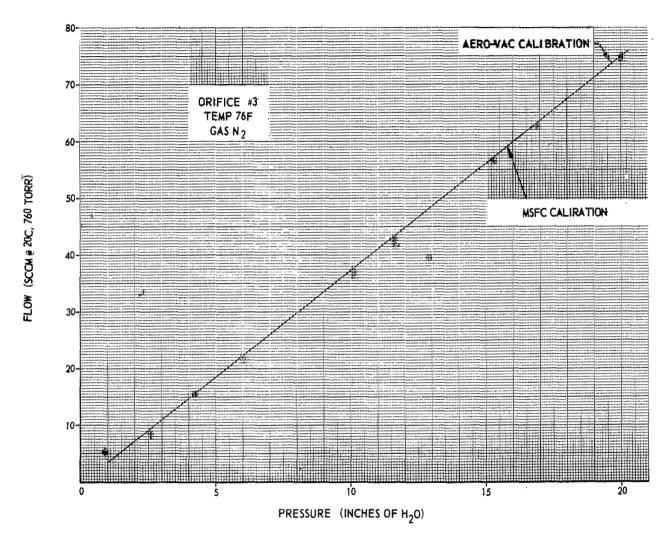


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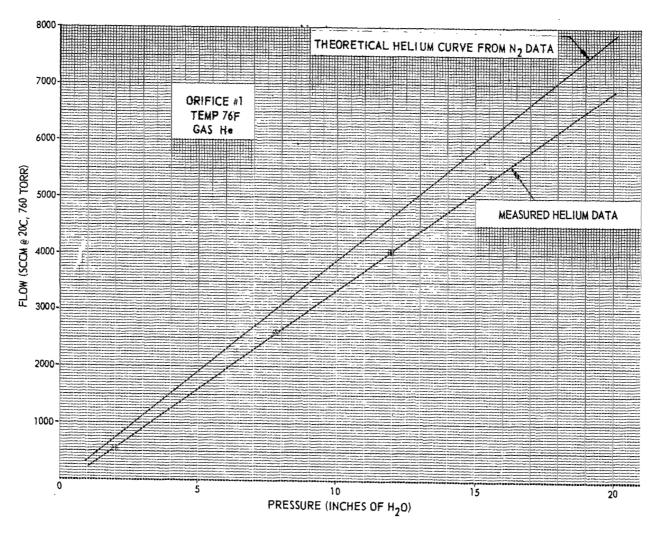


Figure A-2. Helium data and theoretical curve.

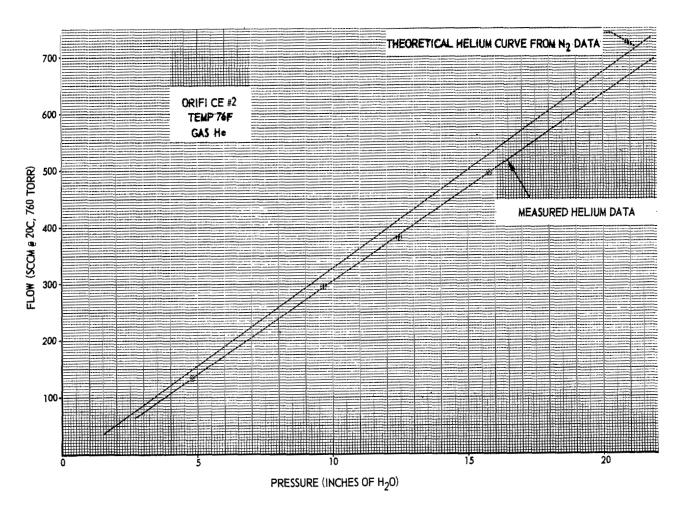


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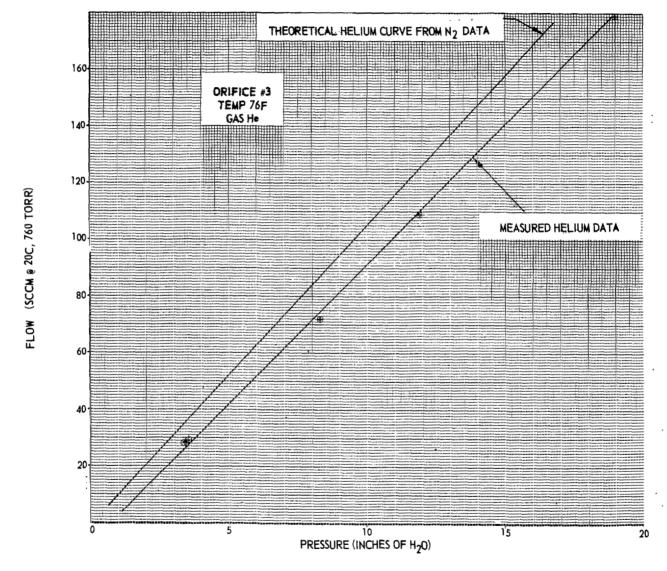


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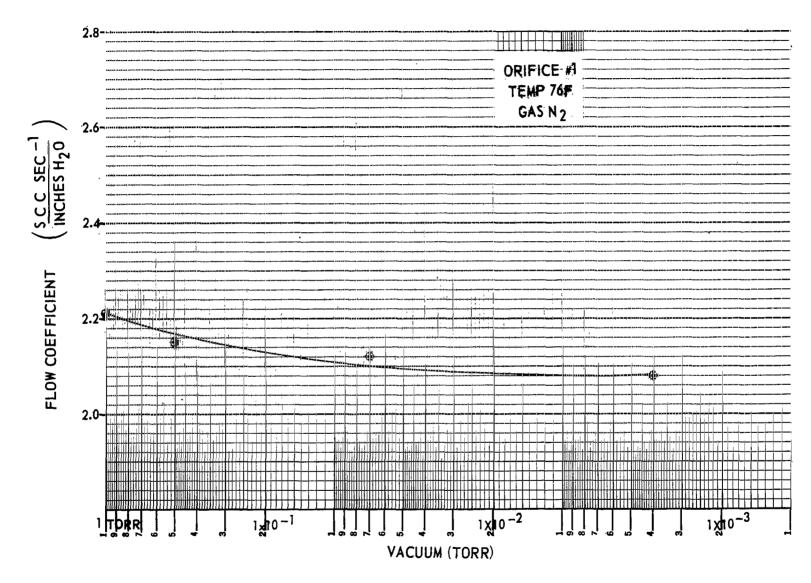


Figure A-3. Effect of pressure variation.

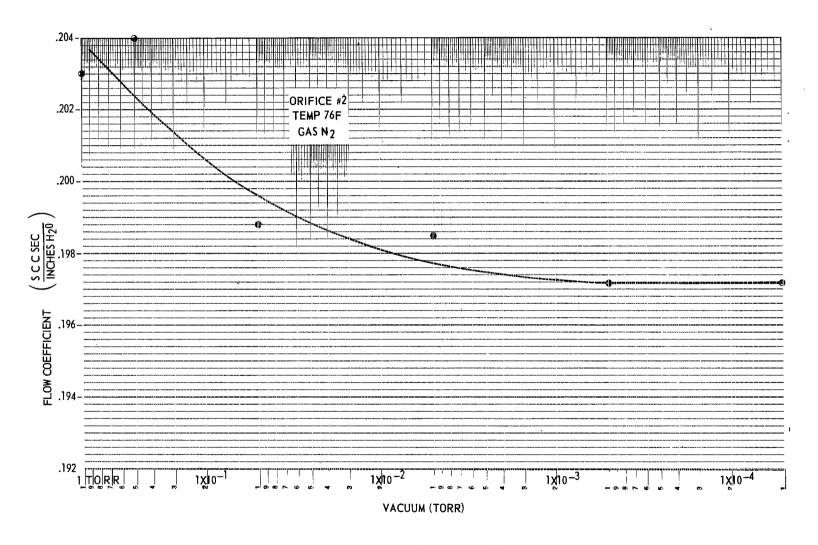


Figure A-3. (Continued).

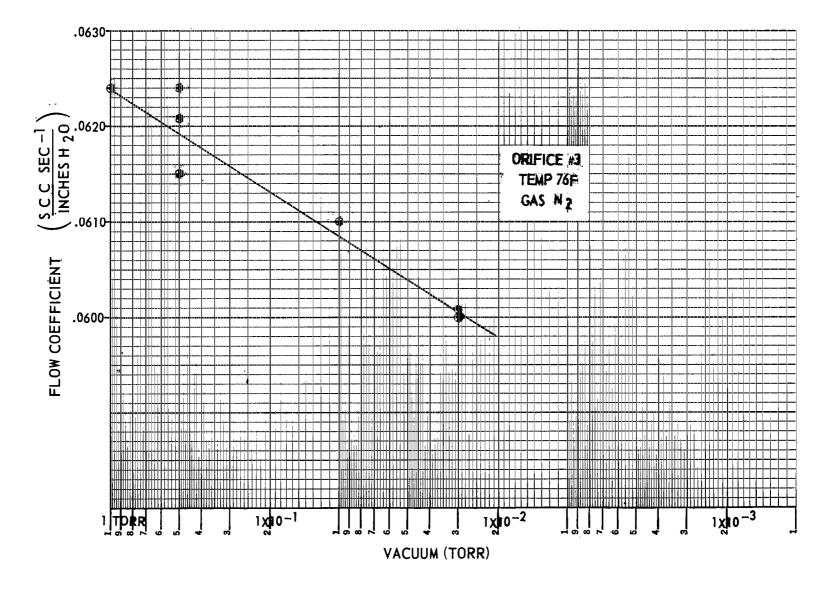


Figure A-3. (Concluded).

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